Fluid-structure interactions: one-field monolithic fictitious domain method and its parallelization

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- Fluid-structure interaction (FSI) is the interaction of some movable or deformable structure with a surrounding fluid flow.
- Fluid-structure interaction exists in its various forms in both natural systems and man-made objects.
- For doing the FSI research or simulation, we test the developed algorithms on benchmark problems which is simpler than the actural problems.

Fluid-Structured Interaction for natural system 1



• The corresponding benchmark problem: oscillating leaflet in 2D channel flow.



Fluid-Structured Interaction for natural system 2

FSI for natural system: 2. ground water interaction with soil



 FSI for engineered systems: 1. modeling behavior of offshore platforms with the ocean

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Figure 3a: Ocean wind power generator impacted by a tsunami wave using MSC Dytran [5]



Figure 3b: Ocean wind power generator impacted by a tsunami wave using MSC Dytran [5]

• Flight characteristics of aircraft.



• The corresponding benchmark problem: flow-induced vibration of an elastic splitter plate.



• FSI for engineered systems: 3. dams with reservoirs.



• The corresponding benchmark problem:



(c) Dam-break flow through an elastic gate

FSI for engineered systems: 3, bioengineering:



Fluid-Structured Interaction for this work

- In this work, FSI simulations use Fictitious Domain Method (FDM).
- We intend to speed up the simulation by parallelizing the algorithm.
- FDM uses two meshes to represent the fluid and solid separately.



The methods

• FDM approach solves for both velocities in the whole domain (fluid plus solid) and update the displacement of the solid simultaneously via a distributed Lagrange multiplier (DLM) to enforce the consistency of velocity/displacement in the overlapped solid domain.



• The solid is represented by a (linear) triangular mesh, while the mesh for the background fluid is (qudratic) rectangular.

- The existing sequential FDM code for Fluid-Structure Interaction takes months to complete a 3D simulation (with low resolution).
- By parallelizing the computations for background fluid mesh, we hope to reduce the simulation time from months to few days.
- The parallel algorithm is designed based on the data structure and parallelism provided by software package PARAMESH.

• $\Omega_t^f \in \mathbb{R}^d$ and $\Omega_t^s \in \mathbb{R}^d$ (d = 2 in Figure) denote the fluid and solid respectively which are time dependent regions.



• $\Omega_t^s \cup \Omega_t^f$ is the fixed domain and $\Gamma_t = \partial \Omega_t^f \cap \Omega_t^s$ is the moving interface between fluid and solid.

- All subscripts, such as *i*, *j*, *k*, represent spatial dimension. In addition, the repeated indices are implicitly summed over.
- u_i^f and u_i^s denote the velocity components of fluid and solid respectively, σ_{ij}^f and σ_{ij}^s denote the stress tensor components of fluid and solid respectively, and $(u_i^s)^n$ is a solid velocity component at time t^n .

Governing equation: fluid equation

- We assume an incompressible fluid governed by the following equations in fluid domain Ω_i^f
 - Momentum equation:

$$\rho^f \frac{Du_i^f}{Dt} - \frac{\partial \sigma_{ij}^f}{\partial x_j} = \rho^f g_i.$$
(1)

Continuity equation:

$$\frac{\partial u_j^f}{\partial x_j} = 0 \tag{2}$$

• Incompressible Newtonian fluid on fluid domain Ω^f :

$$\sigma_{ij}^{f} = \mu^{f} \left(\frac{\partial u_{i}^{f}}{\partial x_{j}} + \frac{\partial u_{j}^{f}}{\partial x_{i}} \right) - p^{f} \delta_{ij} = \tau_{ij}^{f} - p^{f} \delta_{ij}$$
(3)

Governing equation: solid equation

- On the solid domain, we assume an incompressible solid is governed by the following equations in solid domain Ω^s_i:
 - Momentum equation:

$$\rho^{s} \frac{Du_{i}^{s}}{Dt} - \frac{\partial \sigma_{ij}^{s}}{\partial x_{j}} = \rho^{s} g_{i}.$$

$$\tag{4}$$

• Continuity equation:

$$\frac{\partial u_j^s}{\partial x_j} = 0 \tag{5}$$

• Incompressible viscous-hyperelastic solid on solid domain Ω^s

$$\sigma_{ij}^{s} = \mu^{s} \left(\frac{\partial x_{i}^{s}}{\partial X_{k}} \frac{\partial x_{j}^{s}}{\partial X_{k}} \right) - p^{s} \delta_{ij} = \tau_{ij}^{s} - p^{s} \delta_{ij}$$
(6)

• Note that the above equations describe an incompressible neo-Hookean model which is suitable for large displacements.

Governing equation: boundary and initial conditions

• On the interface boundary Γ_t :

$$u_i^f = u_i^s \tag{7}$$

$$\sigma_{ij}^f n_j^s = \sigma_{ij}^s n_j^s$$

• Dirichlet and Neumann boundary conditions may be imposed for the fluid:

$$u_i^f = \bar{u}_i^s$$
 on Γ^D (8)
 $\sigma_{ij}^f n_j = \bar{h}_i$ on Γ^N

• The initial conditions are typically set as:

$$u_{i}^{f}\Big|_{t=0} = u_{i}^{s}\Big|_{t=0} = 0$$
(9)

• Let
$$(u,v)_\omega = \int_\omega uv d\omega$$
, and

$$u_{i} = \begin{cases} u_{i}^{f} \text{ in } \Omega_{t}^{f} \\ u_{i}^{s} \text{ in } \Omega_{t}^{s} \end{cases} \qquad p_{i} = \begin{cases} p_{i}^{f} \text{ in } \Omega_{t}^{f} \\ p_{i}^{s} \text{ in } \Omega_{t}^{s} \end{cases}$$
(10)

• Performing the following symbolic operation to obtain the spatial discretization.

(Eq. (1), v_i) $_{\Omega_t^f}$ - (Eq.(2), q) $_{\Omega_t^f}$ + (Eq. (4), v_i) $_{\Omega_t^s}$ - (Eq. (5), q) $_{\Omega_t^s}$ for independent test functions $v_i \in H_0^1(\Omega)$ and $q \in L^2(\Omega)$ Integrating the stress terms by parts, using constitutive equations (3) and (6) and boundary condition (10), gives the following weak form for the FSI system. Find $u_i \in H^1(\Omega)$ and $p \in L^2_0(\Omega)$ such that

$$\rho^{f} \left(\frac{Du_{i}}{Dt}, v_{i}\right)_{\Omega} + \left(\tau_{ij}^{f}, \frac{\partial v_{i}}{\partial x_{j}}\right)_{\Omega} - \left(p, \frac{\partial v_{j}}{\partial x_{j}}\right)_{\Omega} - \left(\frac{\partial u_{j}}{\partial x_{j}}, q\right)_{\Omega}$$
(11)
+ $\left(\rho^{s} - \rho^{f}\right) \left(\frac{Du_{i}}{Dt}, v_{i}\right)_{\Omega_{t}^{s}} + \left(\tau_{ij}^{s}, \frac{\partial v_{i}}{\partial x_{j}}\right)_{\Omega_{t}^{s}}$
= $(\bar{h}_{i}, v_{i})_{\Gamma^{N}} + \rho^{f}(g_{i}, v_{i})_{\Omega} + (\rho^{s} - \rho^{f})(g_{i}, v_{i})_{\Omega_{t}^{s}}$

for every $v_i \in H_0^1(\Omega)$ and $q \in L^2(\Omega)$.

Discretization in time

 $\frac{D}{Dt}$ represents the total derivative of time, and

$$\frac{Du_i}{Dt} = \frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} \quad \text{in} \quad \Omega \quad (12)$$

$$\frac{Du_i^s}{Dt} = \frac{\partial u_i^s}{\partial t} + u_j \frac{\partial u_i^s}{\partial x_j} \quad \text{in} \quad \Omega^s \quad (13)$$

Using backward finite difference, equation (12) become

$$\rho^{f} \left(\frac{u_{i} - u_{i}^{n}}{\Delta t} + u_{j} \frac{\partial u_{i}}{\partial x_{j}}, v_{i} \right)_{\Omega} + \left(\tau_{ij}^{f}, \frac{\partial v_{i}}{\partial x_{j}} \right)_{\Omega}$$

$$- \left(\rho, \frac{\partial v_{j}}{\partial x_{j}} \right)_{\Omega} - \left(\frac{\partial u_{j}}{\partial x_{j}}, q \right)_{\Omega}$$

$$+ \left(\rho^{s} - \rho^{f} \right) \left(\frac{u_{i} - u_{i}^{n}}{\Delta t}, v_{i} \right)_{\Omega^{s}_{n+1}} + \left(\tau_{ij}^{s}, \frac{\partial v_{i}}{\partial x_{j}} \right)_{\Omega^{s}_{n+1}}$$

$$= \left(\bar{h}_{i}, v_{i} \right)_{\Gamma^{N}} + \rho^{f} (g_{i}, v_{i})_{\Omega} + \left(\rho^{s} - \rho_{i}^{f} \right) (g_{i}, v_{i})_{\Omega^{s}_{n+1} + \frac{1}{2}} = \left(\frac{14}{2} \right) \left($$

Discretization in time: two step splitting

Equation (14) is separated into convection part and diffusion part by the splitting method

Convection step

$$\rho^{f} \left(\frac{u_{i}^{\star} - u_{i}^{n}}{\Delta t} + u_{j}^{\star} \frac{\partial u_{i}^{\star}}{\partial x_{j}}, v_{i} \right)_{\Omega} = 0$$
(15)

Diffusion step

$$\rho^{f} \left(\frac{u_{i} - u_{i}^{*}}{\Delta t}, v_{i}\right)_{\Omega} + \left(\tau_{ij}^{f}, \frac{\partial v_{i}}{\partial x_{j}}\right)_{\Omega}$$
(16)
$$- \left(\rho, \frac{\partial v_{j}}{\partial x_{j}}\right)_{\Omega} - \left(\frac{\partial u_{j}}{\partial x_{j}}, q\right)_{\Omega}$$
$$+ \left(\rho^{s} - \rho^{f}\right) \left(\frac{u_{i} - u_{i}^{n}}{\Delta t}, v_{i}\right)_{\Omega_{n+1}^{s}} + \left(\tau_{ij}^{s}, \frac{\partial v_{i}}{\partial x_{j}}\right)_{\Omega_{n+1}^{s}}$$
$$= (\bar{h}_{i}, v_{i})_{\Gamma^{N}} + \rho^{f}(g_{i}, v_{i})_{\Omega} + (\rho^{s} - \rho^{f})(g_{i}, v_{i})_{\Omega_{n+1}^{s}}$$
$$= -\infty$$

Discretization in spatial variables: finite element

- For our space- and time-dependent PDEs we use finite element method (FEM) for approxiamting the spatial variables to compute the approximate solution (evoled with time).
- The solution u(x, y, t) of PDEs can be approximated by a function $u_h(x, y, t)$ using linear combinations of basis functions ψ_i according to the following expressions:

$$u pprox u_h$$
 and $u_h = \sum u_i \psi_i$

where u_i denotes the coefficients of the functions that approximate u with u_h .



Discretization in spatial variables: finite element

• The spatial discretization for fluid domain use P_1P_2 rectangular element (the Taylor-Hood element). The solid domain is discretized by P_1 triangular elements. The corresponding finite element spaces are

$$egin{array}{rcl} V^h(\Omega^h) &=& span\{\psi_1,...,\psi_{N^u}\}\subset H^1(\Omega)\ L^h(\Omega^h) &=& span\{\phi_1,...,\phi_{N^p}\}\subset L^2(\Omega) \end{array}$$



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Discretization in spatial variables: finite element

• For the solid domain

$$V^{sh}(\Omega^{sh}_{n+1})= extsf{span}\{\phi^s_1,...,\phi^s_{N^s}\}\subset H^1(\Omega^s_{n+1}).$$



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- The approximate solutions for velocities and pressure are $\mathbf{u}^{h}(\mathbf{x}) = \sum_{i=1}^{N^{u}} \mathbf{u}(\mathbf{x}_{i})\psi_{i}(\mathbf{x})$ and $p^{h}(\mathbf{x}) = \sum_{i=1}^{N^{p}} p(\mathbf{x}_{i})\phi_{i}(\mathbf{x})$, respectively.
- The approximate solutions for solid domain is $\mathbf{u}^{sh}(\mathbf{x}) = \sum_{i=1}^{N^s} \sum_{j=1}^{N^u} \mathbf{u}(\mathbf{x}_j) \phi_j(\mathbf{x}_i^s) \phi_i^s(\mathbf{x})$

• The linear system arising from the above finite element discretization is

$$\begin{bmatrix} \mathbf{A} & \mathbf{B} \\ \mathbf{B}^T & \mathbf{0} \end{bmatrix} \begin{bmatrix} \mathbf{u} \\ \mathbf{p} \end{bmatrix} = \begin{bmatrix} \mathbf{b} \\ \mathbf{0} \end{bmatrix},$$
(17)

where $\mathbf{A} = \mathbf{M}/\Delta t + \mathbf{K} + \mathbf{D}^T (\mathbf{M}^s / \Delta t + \mathbf{K}^s) \mathbf{D}$, and $\mathbf{b} = f + \mathbf{D}^T f^s + \mathbf{M} \mathbf{u}^* / \Delta t + \mathbf{D}^T \mathbf{M}^s \mathbf{D} \mathbf{u}^n / \Delta t$. Furthermore, **D** is the isoparametric interpolation matrix, **M** and **M**^s are mass matrices, **K** and **K**^s the stiffness matrices from discretization of the terms in the weak form related to fluid and solid, respectively. **B** from discretization of the linear functional related to the pressure variable. f and f^s are force vectors.

Overall solution algorithm

The solution algorithm at each time step is described as follows

Given the solid configuration (x^s)ⁿ and velocity field at the time step n

$$\mathbf{u}^{n} = \begin{cases} (\mathbf{u}^{f})^{n} & \text{in} & \Omega^{f} \\ (\mathbf{u}^{s})^{n} & \text{in} & \Omega^{s} \end{cases}$$
(18)

- Oiscretize the convection equation and solve it to get an intermediate velocity u*.
- In diffusion step compute the interpolation matrix and solve linear system (17) using u^{*} and (u^s)ⁿ as initial values to get velocity field uⁿ⁺¹ at the time step n + 1.
- Compute solid velocity $(\mathbf{u}^s)^{n+1} = \mathbf{D}\mathbf{u}^{n+1}$ and update the solid mesh by $(\mathbf{x}^s)^{n+1} = (\mathbf{x}^s)^n + \Delta t (\mathbf{u}^s)^{n+1}$, then go to step (1) for the next time step.

- The parallelization implementation is carried out in 'Campfire', a software tool developed by Goodyear et al.
- In Campfire, the data structure and parallelism are provided by software package PARAMESH.
- At this stage we assess all the parallel issues for the fluid-structure cases on structured uniform grid in Campfire.

Data type: blocks

The basic data storage units in PARAMESH are blocks (shown as below). Each block consists of $n \times n$ cells, where generally n is an even integer. The outer layer cells of the block are guardcells which are used for communicating/exchanging data from neighboring blocks.



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In finite element implementation we view each cell as an rectangular element, consisting of 9 nodes for 2D domain.



Figure: nodes in a cell, viewed as an element in our implementation.

Domain division

At the setup stage, the fluid domain is divided into blocks. Then each processor is assigned for one block.





Figure: Graphic demonstration for four 2×2 block which have boundary cells and the guard cells containing the cells from neighbouring blocks where \mathbb{R}_{2} and $\mathbb{R$

- In our parallel implementation, each processor computes the whole stiffness and mass matrices for the solid mesh.
- On fluid domain the computations of element matrices are local for each process, which is one of the main source of the algorithm parallelism.
- The assembly of the global finite element matrix from element matrices is carried out in each process. In this way each process has a part of the rows of the global discretization matrix which are corresponding to the variables owned by the block in the process.
- To guarantee the correctness of the parallel computation, the largest radius of the triangle element in solid mesh can not be greater than two times of spatial grid space Δx or Δy . Therefore, we use two layers of guardcells for parallel communications.

- The linear system (17) is solved using GMRES, an iterative linear system solver.
- The interpolation of solid matrix (D^T(M^s/Δt + K^s)D in (17)) into fluid matrix is not done explicitly. Instead we compute the sum of the two products (M/Δt + K)v and (D^T(M^s/Δt + K^s)D)v in the matrix-vector multiplication step of GMRES. Both computations are local with respect to the block in a process.
- In each iteration there are one matrix-vector multiplication and two inner products.
- At the end of each iteration, communications between neighboring processes must be carried out so that the matrix-vector multiplication is the same as the result in serial computation.

GMRES preconditioner

 To speed up GMRES we use the incomplete LU decomposition of the matrix

$$\begin{bmatrix} \mathbf{A}' & \mathbf{0} \\ \mathbf{0} & \mathbf{I} \end{bmatrix}$$
(19)

as the preconditioner, where $\mathbf{A}' = \mathbf{M}/\Delta t + \mathbf{K}$.

- The parallel version of the above preconditioner omits the connections between the variables located in different blocks and the rows corresponding to nodes at the internal interfaces are [0, ..., 0, 1, 0, ..., 0]. Thus the ILU decomposition in the parallel cases are different from that in the serial cases and the simulations show that the parallel preconditioner is less effective than the serial preconditioner.
- In the cases tested so far, the iteration count for parallel preconditioned GMRES is 30% more than that for the serial preconditioned GMRES.

Case I: sphere in lid-driven cavity flow 2D



Figure: Lid-driven cavity flow and the boundary conditions.

Case I: sphere in lid-driven cavity flow 2D

- We have the 2D parallel code running correctly. We tested the code on the example with fluid mesh resolution 128×128 . The solid mesh contains 31163 elements and 15794 nodes. The elastic modulus is 0.01. The step size is $\Delta t = 0.01$ and we ran 800 time steps.
- The running time for the last 100 time steps and speed up are shown as follows:

last 100 time steps	serial	4	16	64
time (minutes)	3907	1194	404	172
time (minutes)	1	3.27	9.66	22.77

Table: Triathlon results

Case I: sphere in lid-driven cavity flow 2D

• An output example of the simulation:

- We also have test the code for 3D case. The fluid mesh resolution is $32 \times 32 \times 32$, solid mesh contains 48649 elements and 8994 nodes. $\Delta t = 0.001$, 6000 time steps.
- The running time for the last 100 time steps and speed up are shown as follows:

100 time steps	serial	8	64
time (minutes)	8962	1273	315
speedup	1	7.04	28.45

Table: Triathlon results

Case II: sphere in lid-driven cavity flow 3D

• An output example of the simulation:

Case III: An oscillating leaflet in 2D channel flow

• In this example the motion of a leaflet in 2D channel flow is simulated. The flow direction is perpendicular to the leaflet. The elastic modulus of the leaflet is 10^7 , much higher than that in the previous cases. The fluid field is resolved by 384×96 elements and the solid mesh contains 154 elements and 116 nodes. At the entrance and exit of the channel the velocity is set to be

$$u = 15y(2 - y)\sin(2\pi t), \qquad v = 0.$$

The simulation's time step size is $\Delta t = 1 \times 10^{-4}$ and we ran for 10000 time steps.

• The running time from 3000th time step to 7000th time step and the speed up are shown as follows:

middle 2000 time steps	serial	8	32	128
time (minutes)	635	122	60.4	36.7
speed up	1	5.2	10.5	17.3

Table: Triathlon results

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• An output example of the simulation:

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